

# **Pilot Testing of a Membrane System for Post-Combustion CO<sub>2</sub> Capture DE-FE0005795**

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**NETL CO<sub>2</sub> Capture Technology Meeting**

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# Project Overview

**Award name:** Pilot testing of a membrane system for post-combustion CO<sub>2</sub> capture

**Project period:** 10/1/10 to 9/30/15

**Funding:** \$15 million DOE; \$3.75 million MTR

**DOE program manager:** Jose Figueroa

**Participants:** MTR, Babcock & Wilcox, SCS/NCCC, EPRI, Vectren

**Project scope:** Demonstrate a membrane process to capture 20 tons of CO<sub>2</sub>/day (TPD) from a flue gas slipstream of a coal-fired power plant.

**Project plan:** The key project work organized by budget period is as follows:

- BP1 – Membrane optimization through continued slipstream testing on the 1 TPD system and computational evaluation of sweep recycle with B&W
- BP2 – Design and construction of the 20 ton/day system, boiler testing at B&W with CO<sub>2</sub>-laden air; membrane/module optimization and durability testing through continued testing on 1 TPD system
- BP3 – 6-month pilot test of the 20 ton/day system; comparative economic analysis; industrial 1 TPD field test; Vectren case study at 20 MW-scale

# Pros and Cons of a Membrane Post-Combustion Capture Process

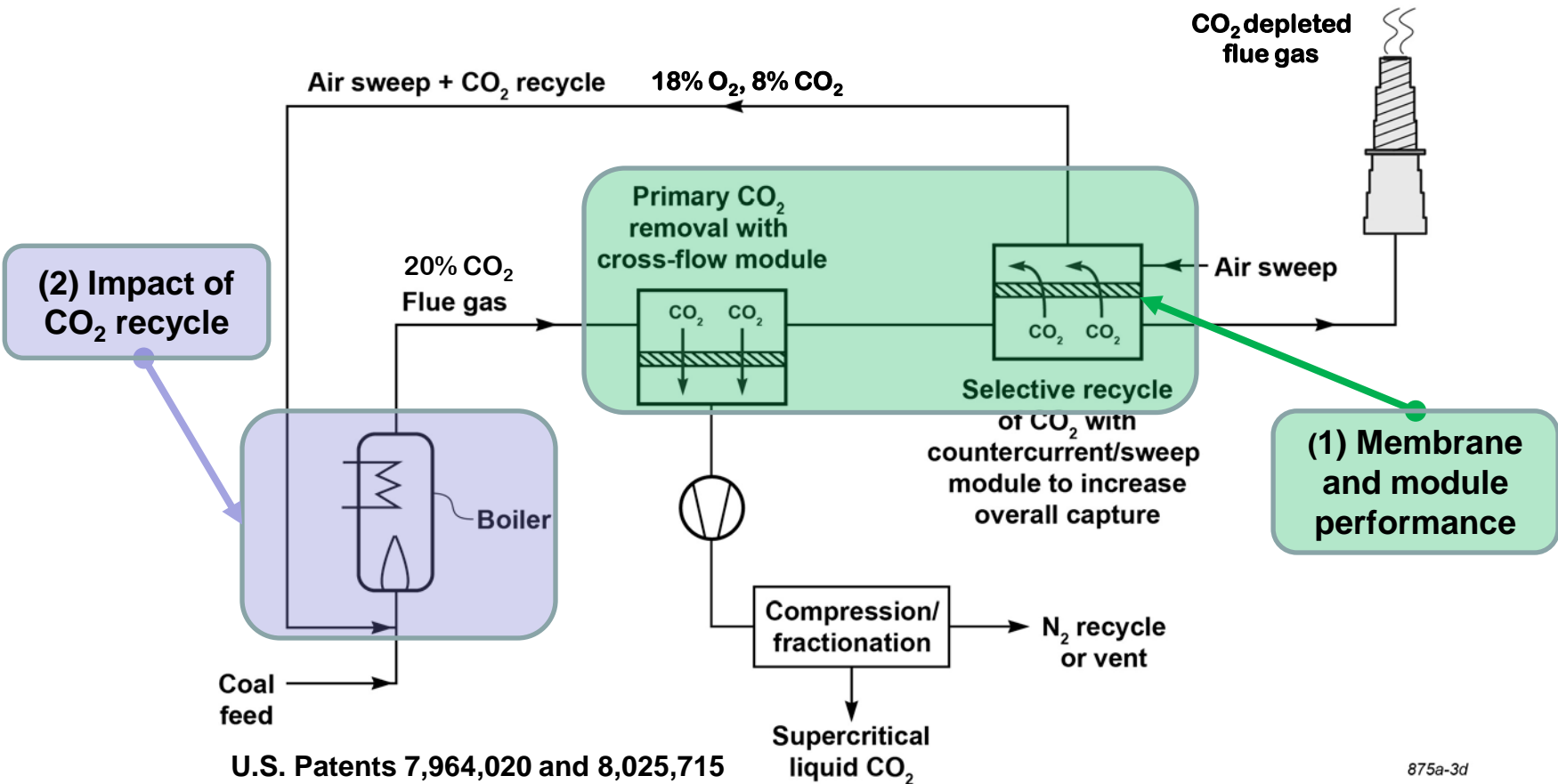
## Benefits:

- No hazardous chemical handling, emissions, or disposal issues
- Not affected by oxygen,  $\text{SO}_x$  or  $\text{NO}_x$ ; co-capture possible
- Water use lower than other technologies (recovers  $\text{H}_2\text{O}$  from flue gas)
- No steam use → no modifications to existing boiler/turbines
- Near instantaneous response; high turndown possible
- Very efficient at partial capture (~60%)

## Challenges:

- How to generate a pressure driving force in an affordable manner?
- Very permeable/low cost membranes required
- Unknown impact of particulate matter on membrane-module lifetime
- Materials and performance challenges for rotating equipment used (blowers, compressors, vacuum pumps)
- Pressure drop and module flow distribution

# MTR CO<sub>2</sub> Capture Process



- Combustion air sweep provides driving force that lowers the capture energy
- Pre-concentrated CO<sub>2</sub> decreases membrane area and power required

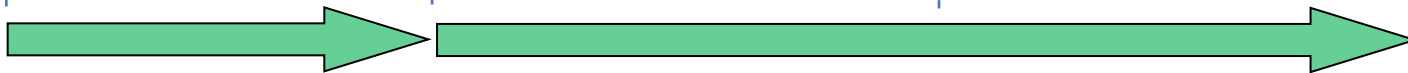
# Timeline of Major Project Tasks



BP1

BP2

BP3



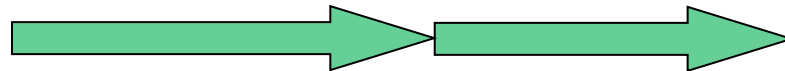
## Optimize Process Design and Complete Systems/Economic Analysis

- In BP1, complete preliminary systems and economic analysis
- In BP2 and 3, evaluate new designs and update economic analysis



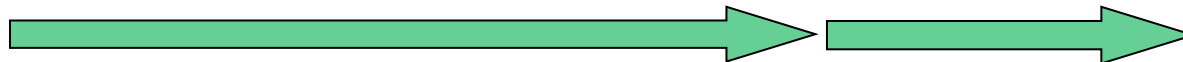
## Continue Membrane Optimization on 1 TPD System

- Run continuous tests at NCCC
- Improve membrane/module performance
- Collect membrane lifetime data



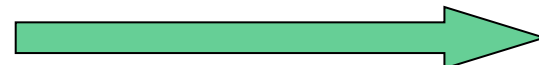
## Boiler Recycle Study

- Evaluate CO<sub>2</sub> recycle with B&W
- Computer modeling in BP1; boiler testing in BP2



## Design/Install/Operate 1 MW Demo (20 TPD)

- Design, build, and install the 20 TPD system at NCCC in BP2
- Run 6+ month test (parametric and SS) in BP3

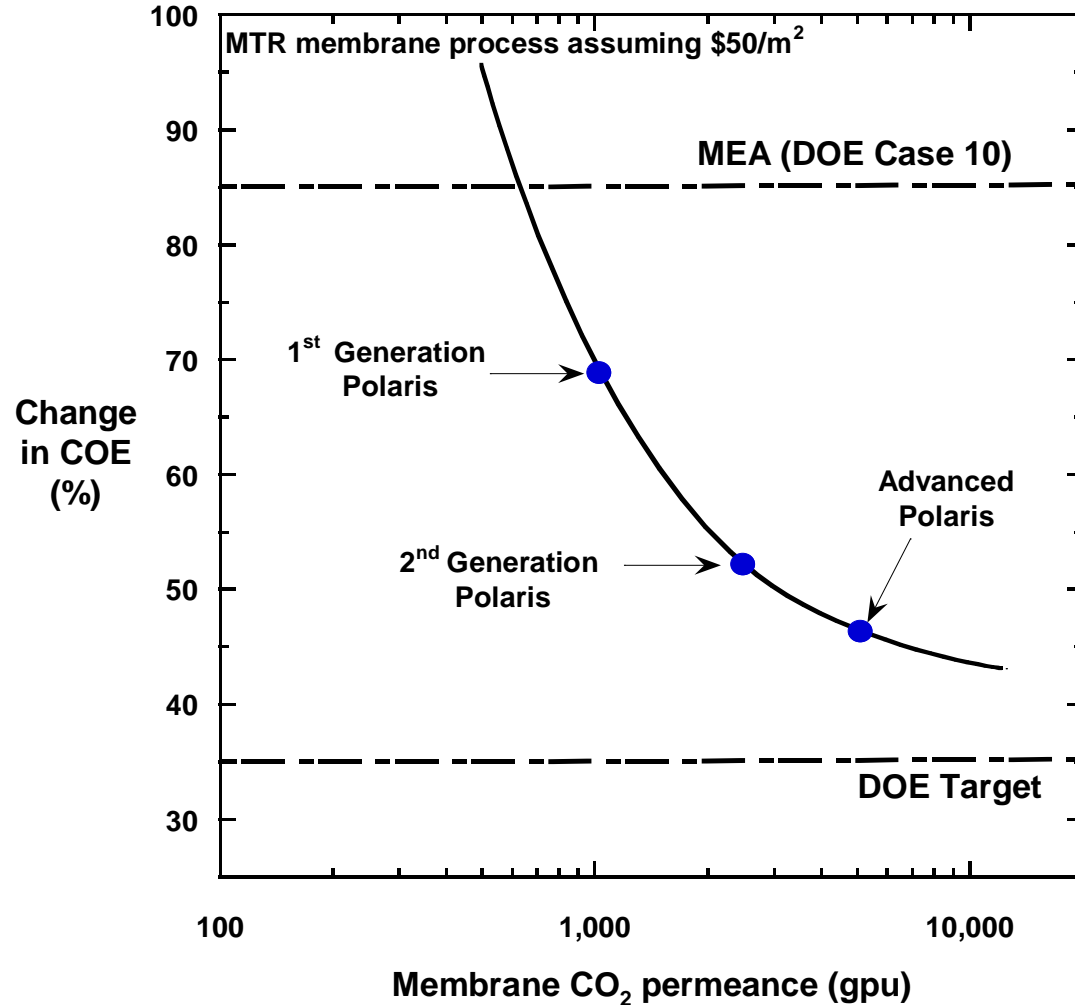


## Industrial CO<sub>2</sub> Capture Test

- Field test CO<sub>2</sub> capture from syngas
- Conduct economic analysis based on test results

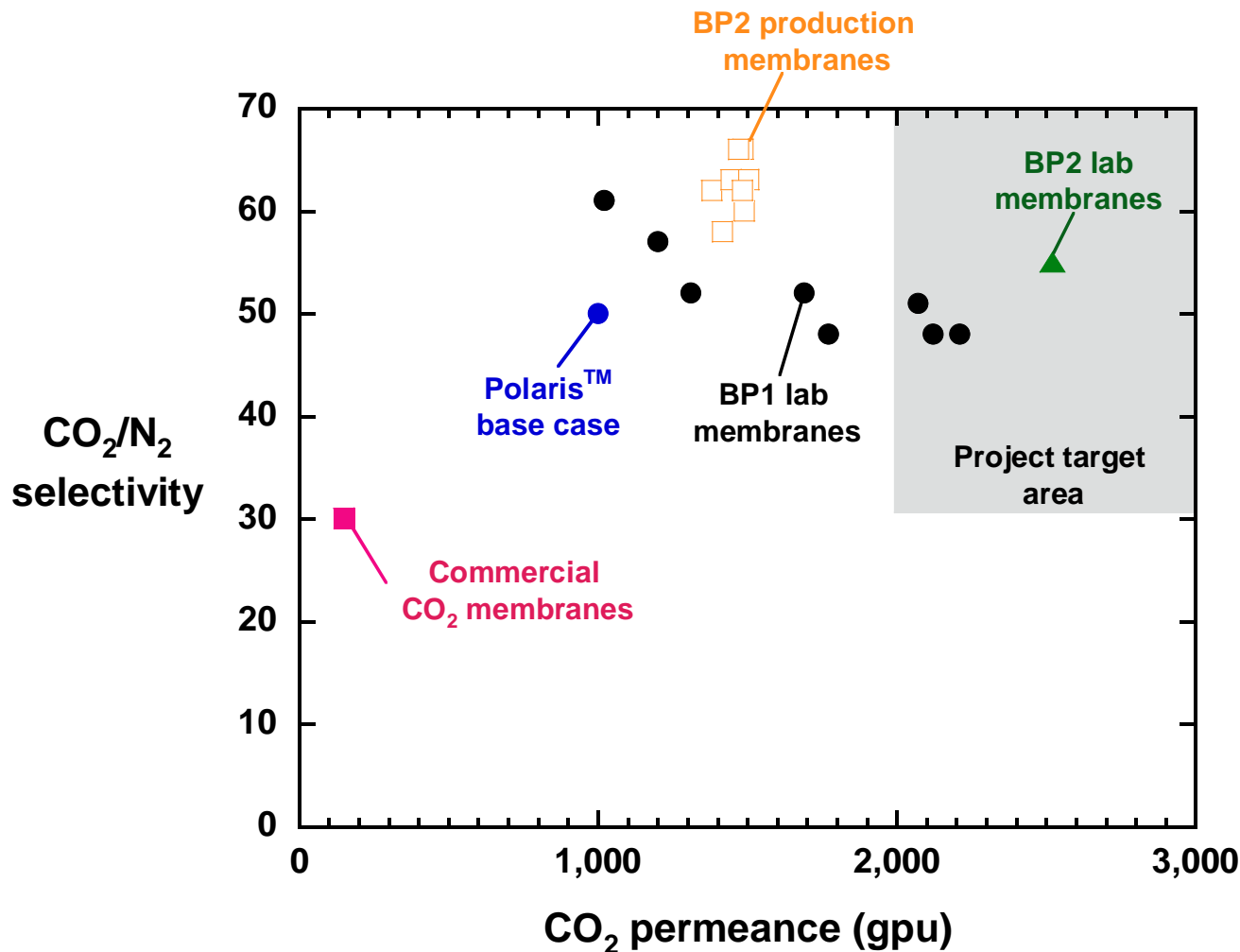
As of 6/30/13, project  
45% complete

# Systems Analysis: Importance of Membrane Improvements



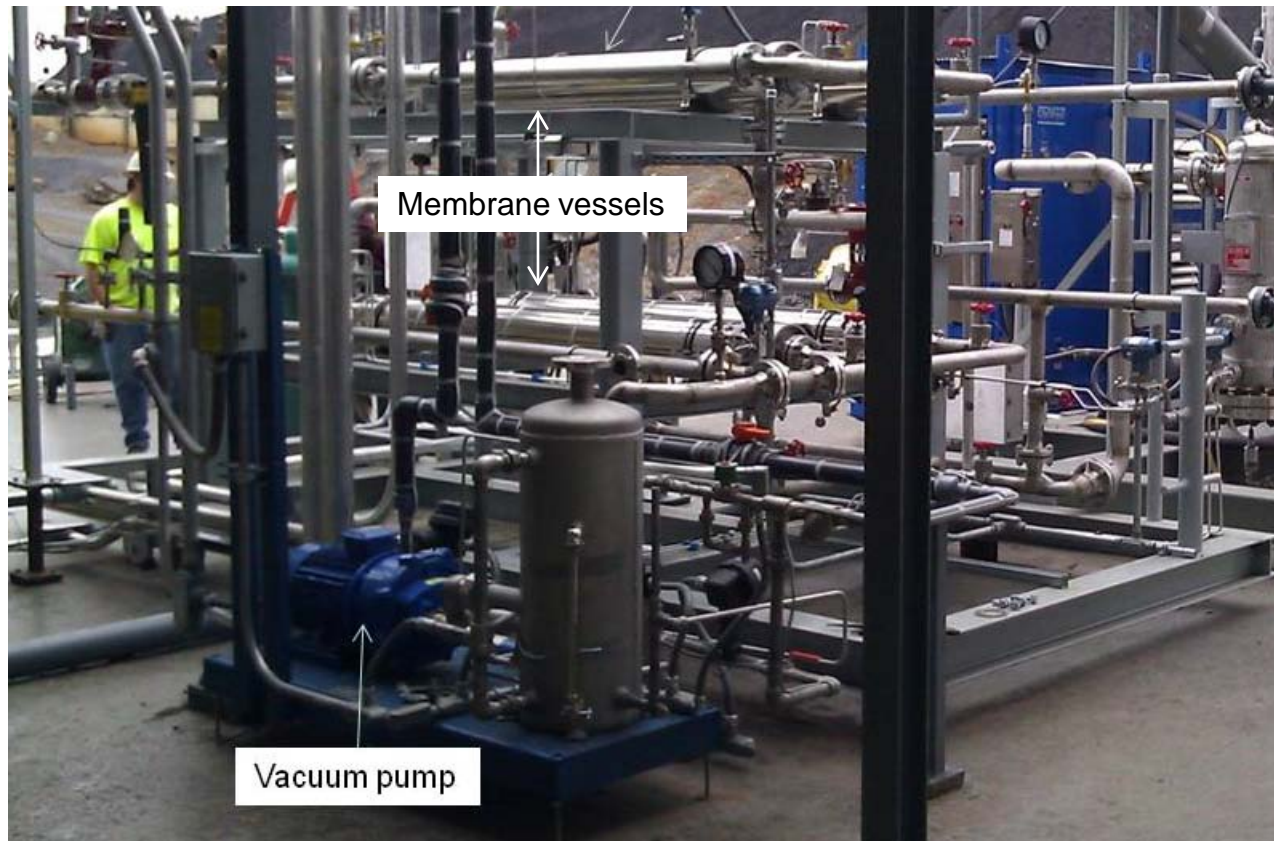
- Study completed in BP1 to meet a project milestone
- All calculations for 90% CO<sub>2</sub> capture use Bituminous Baseline report methodology
- Higher permeance (lower cost) membranes are key to approaching DOE goals
- Results are generally consistent with independent findings reported in DOE report “Current and Future Technologies for Power Generation with Post-Combustion Carbon Capture” (DOE/NETL-2012/1557)

# Membrane Performance Improvements



- Membranes continue to improve
- In addition to lower cost, these improvements are important to shrink the size of the capture system

# 1 TPD System at NCCC

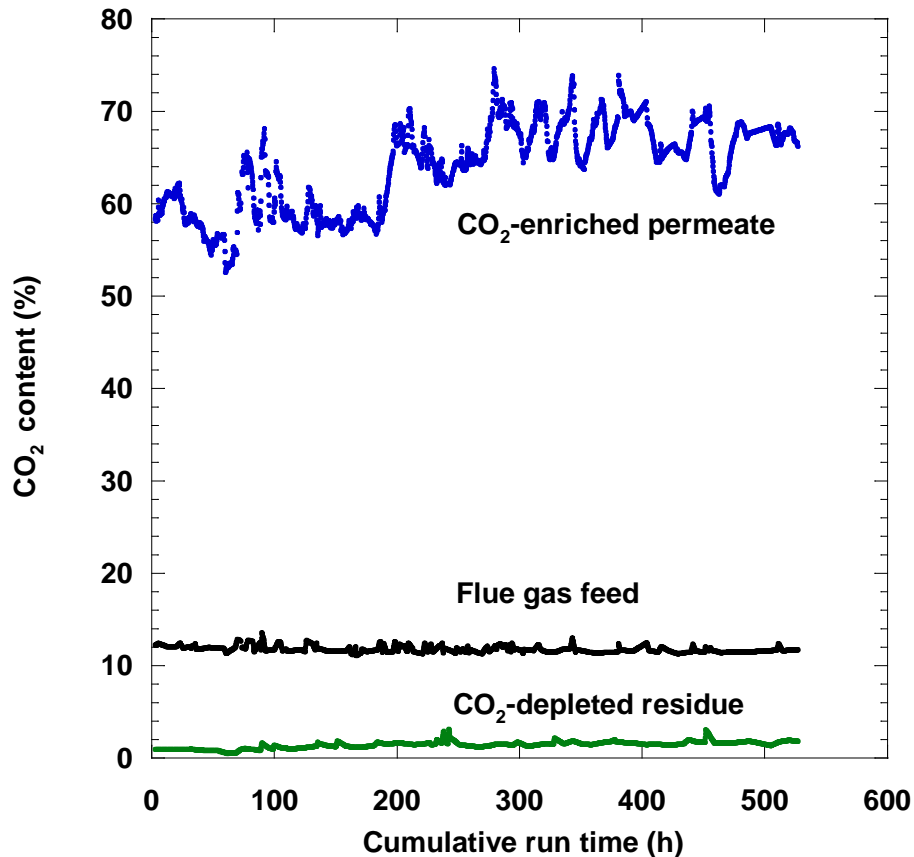


- System is testing vacuum and air sweep membrane steps
- Sized to capture 1 ton CO<sub>2</sub>/day using commercial 40-inch-long modules
- System installed Nov 2011; operation started Spring 2012

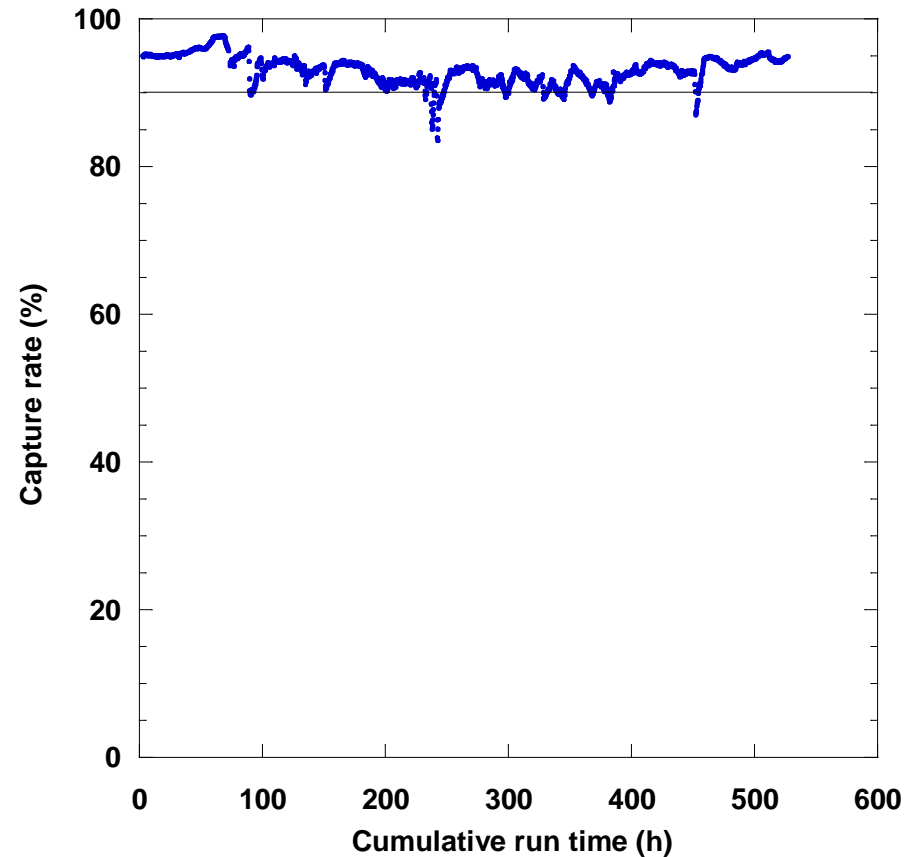


# Sample Results at NCCC

## CO<sub>2</sub> Concentration



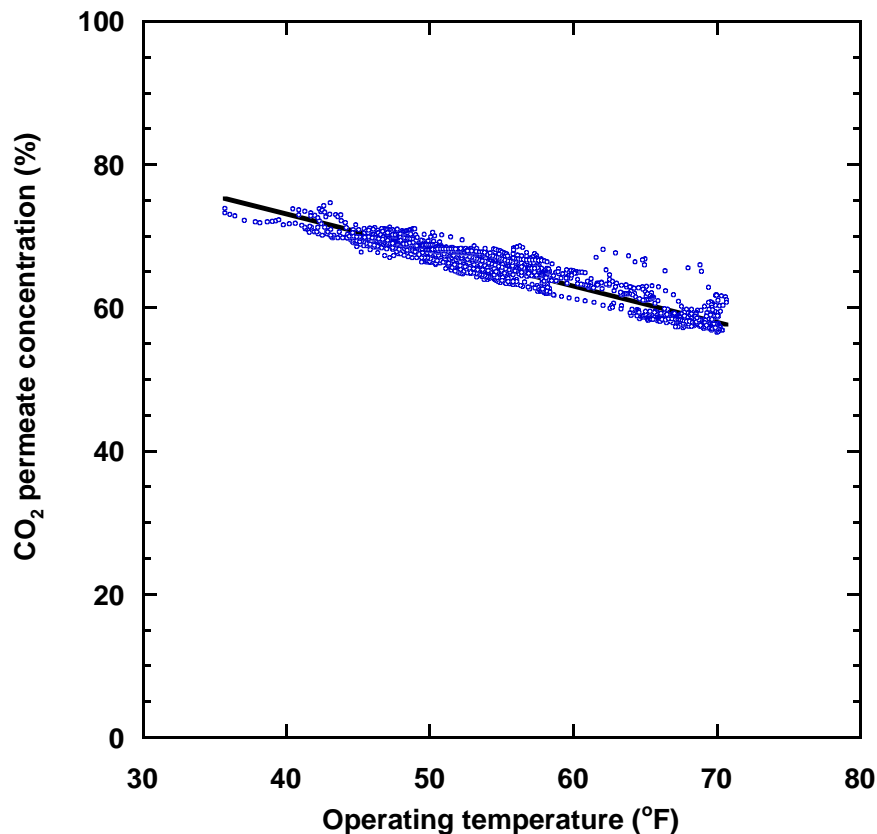
## Capture Rate



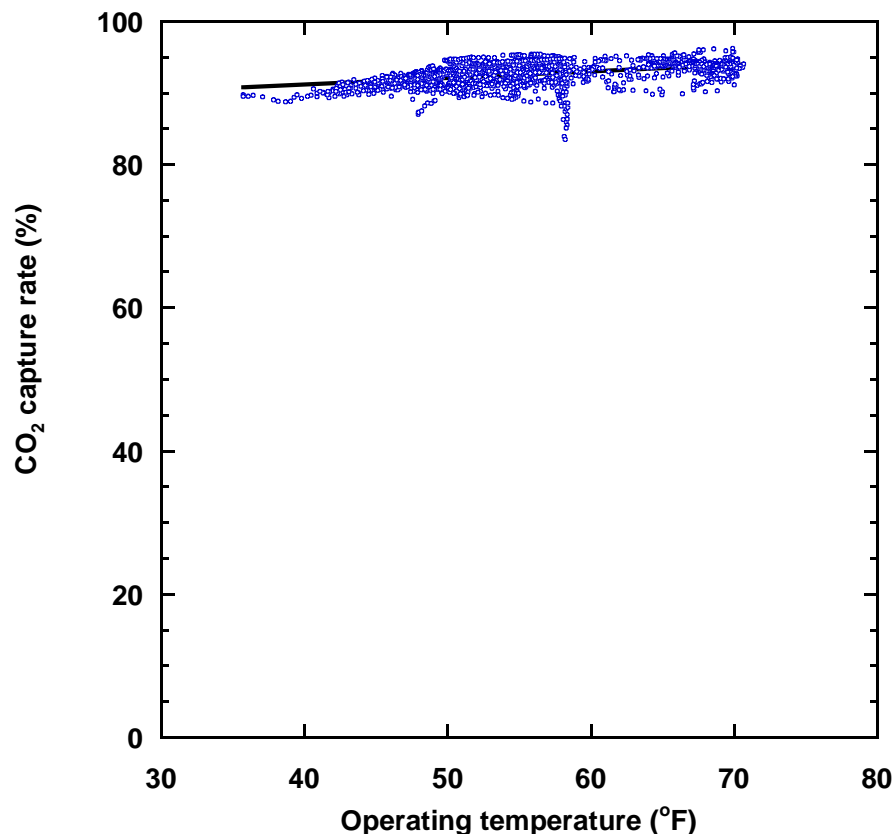
Most concentration fluctuations due to changes in feed gas temperature

# Correlation of CO<sub>2</sub> Purity and Capture Rate With Temperature

## CO<sub>2</sub> Concentration



## Capture Rate



- Higher temperatures yield higher gas permeances, leading to greater CO<sub>2</sub> capture, but at lower purity; could be controlled by switching modules on and offline depending on temperature.

# 1 TPD System: Lessons Learned

- In July 2012, compressor failed due to extensive deposition of unknown material
- NCCC and MTR analyses indicate presence of water soluble sulfur salts (ammonium sulfate/bisulfate, iron sulfate)
- It is believed these salts were created in SCR/FGD operation upstream of the membrane, and were present as aerosols in the flue gas fed to the system
- A more solids-tolerant liquid ring compressor was installed; appears to effectively remove acidic aerosol in sealing water

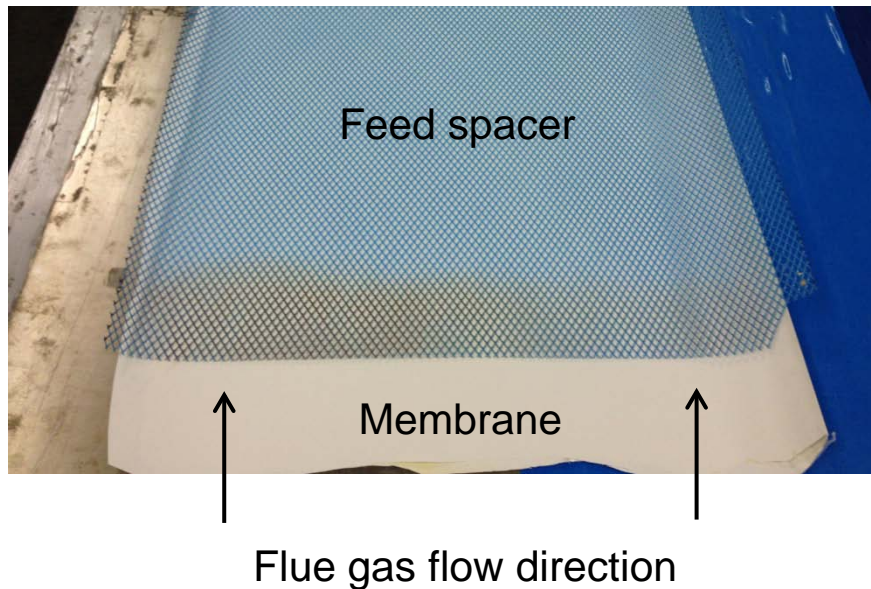


Motor element showing deposition



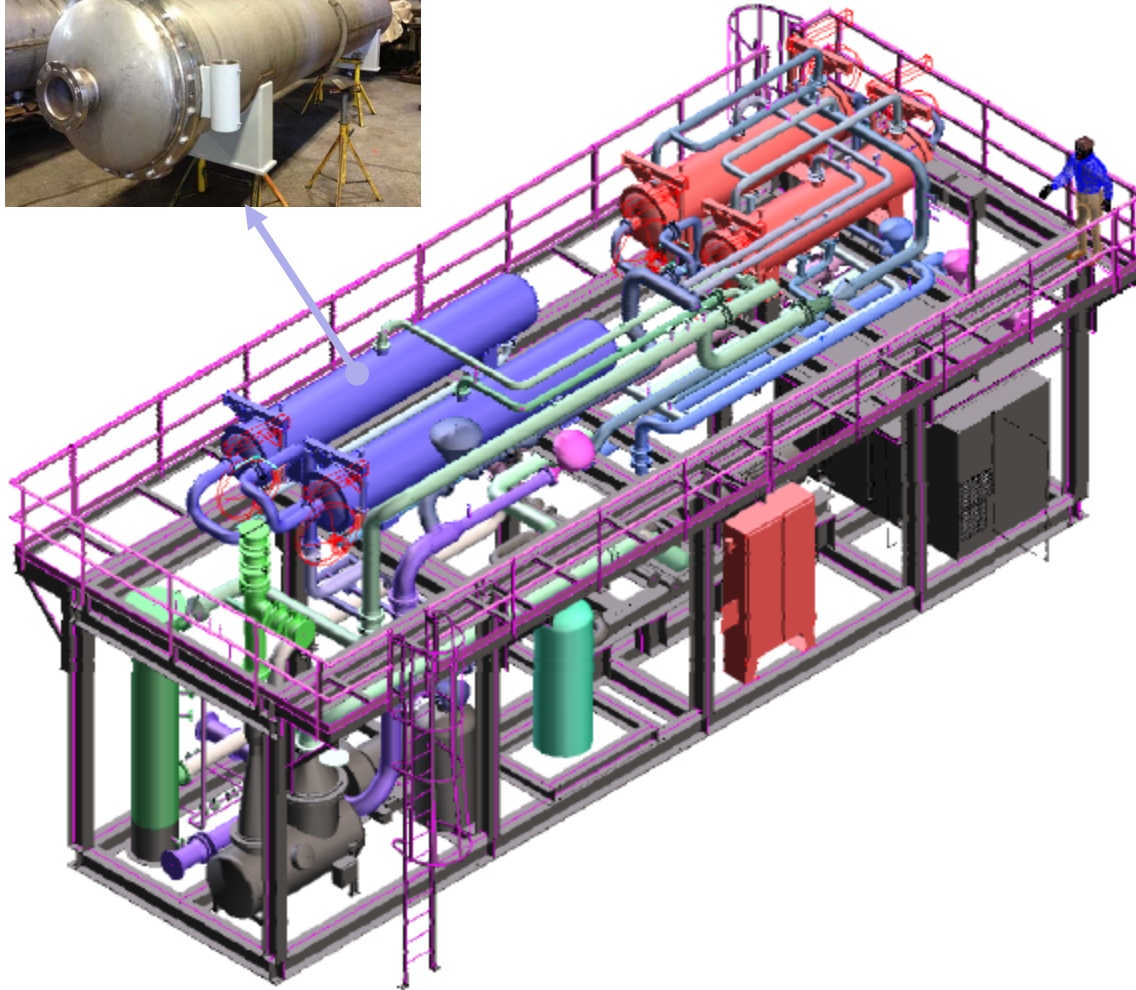
Material dissolved in water

# 1 TPD System: Lessons Learned



- After compressor failure, system continued operating with vacuum only until Sept 2012
- Membranes showed stable performance during this time
- After shutdown at end of Sept, it was found that condensed water with dissolved sulfate salts collect on surface of membrane, and resulted in low CO<sub>2</sub> flux
- To prevent future occurrence, system shutdown procedure changes, and module material solutions developed
- Several startup/shutdown cycles since these changes show stable membrane performance

# 20 TPD System Status



- 20 TPD skid (1 MW<sub>e</sub>) design is complete; now under construction
- Fabrication and site preparation on schedule
- Planned installation at NCCC in 1Q2014, followed by 6 month demonstration
- Will test 2<sup>nd</sup> generation modules designed for low pressure drop while minimizing footprint (cost)



# 20 TPD System Location at NCCC/PC4



Picture courtesy of Mr. Tony Wu, Southern Company

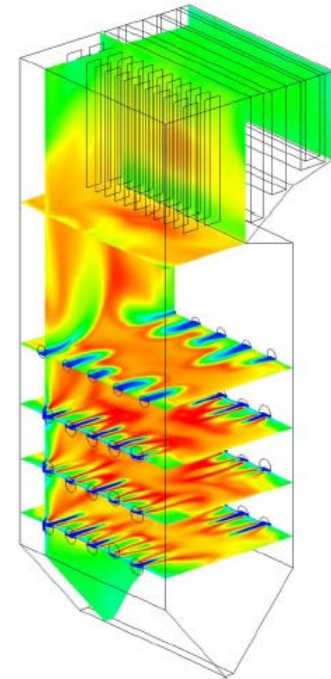
# Impact of CO<sub>2</sub> Recycle on Boiler Performance

## Phase I (BP1) – CFD modeling

- B&W modeled 2 boiler configurations (radiant boiler firing bituminous coal and SWUP firing PRB coal) and 2 sweep recycle cases (constant secondary air flow and constant stoichiometry)
- Main conclusion of modeling study: secondary air laden with CO<sub>2</sub> appears feasible as a retrofit in either of the boiler configurations examined if oxygen mass flow to boiler is fixed

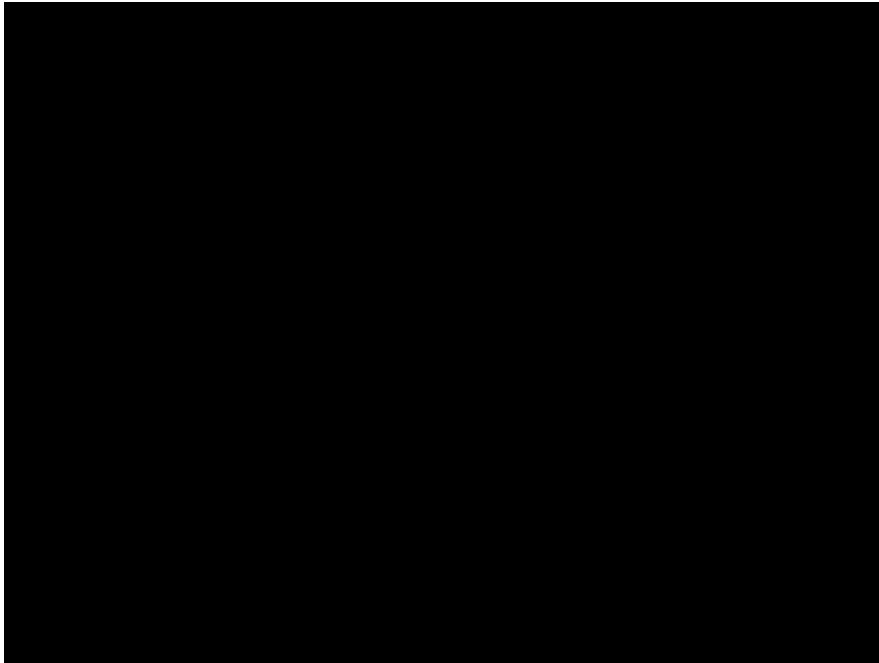
## Phase II (BP2) – Pilot testing

- B&W's SBS-II 1.8 MW<sub>th</sub> pilot boiler operated with CO<sub>2</sub>-laden combustion air
- Two coals evaluated: a western sub-bituminous coal and a highly volatile bituminous coal
- O<sub>2</sub> content of windbox air varied from 21% to 16% through CO<sub>2</sub> dilution
- Monitored flame stability, length, and shape; unburned combustibles in fly ash, and furnace exit gas temperature
- Radiant furnace and convective pass heat absorptions were measured
- Boiler efficiencies for air and sweep firing being determined

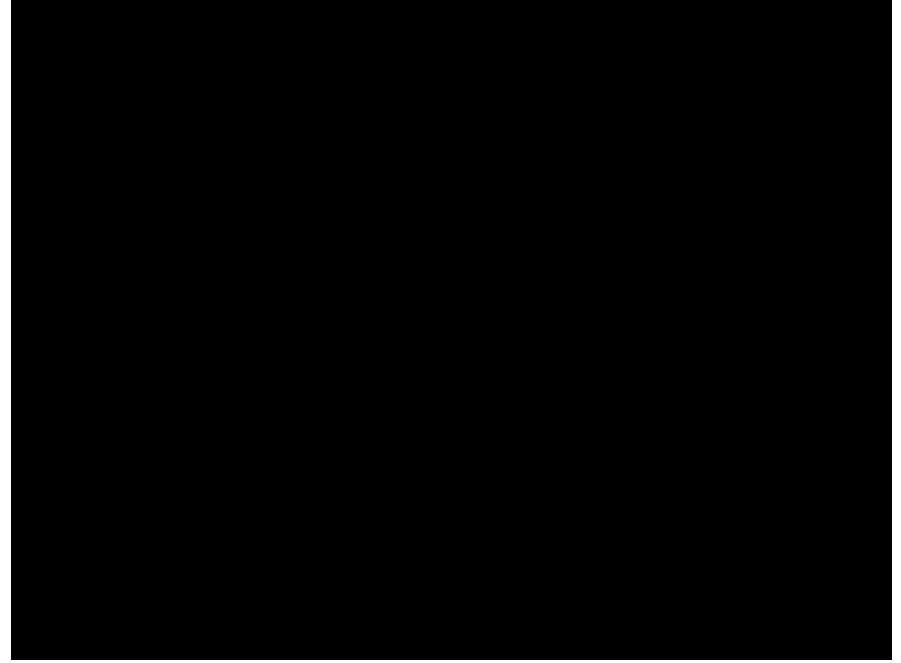


# Baseline and Sweep Air Flames with a Western Sub-Bituminous Coal

**Air-Firing**



**Sweep Air-Firing**



**Conditions:** 5 MMBtu/h with sub-bituminous coal; deep staged flame, stoichiometry 0.8; sweep air is 18% O<sub>2</sub>

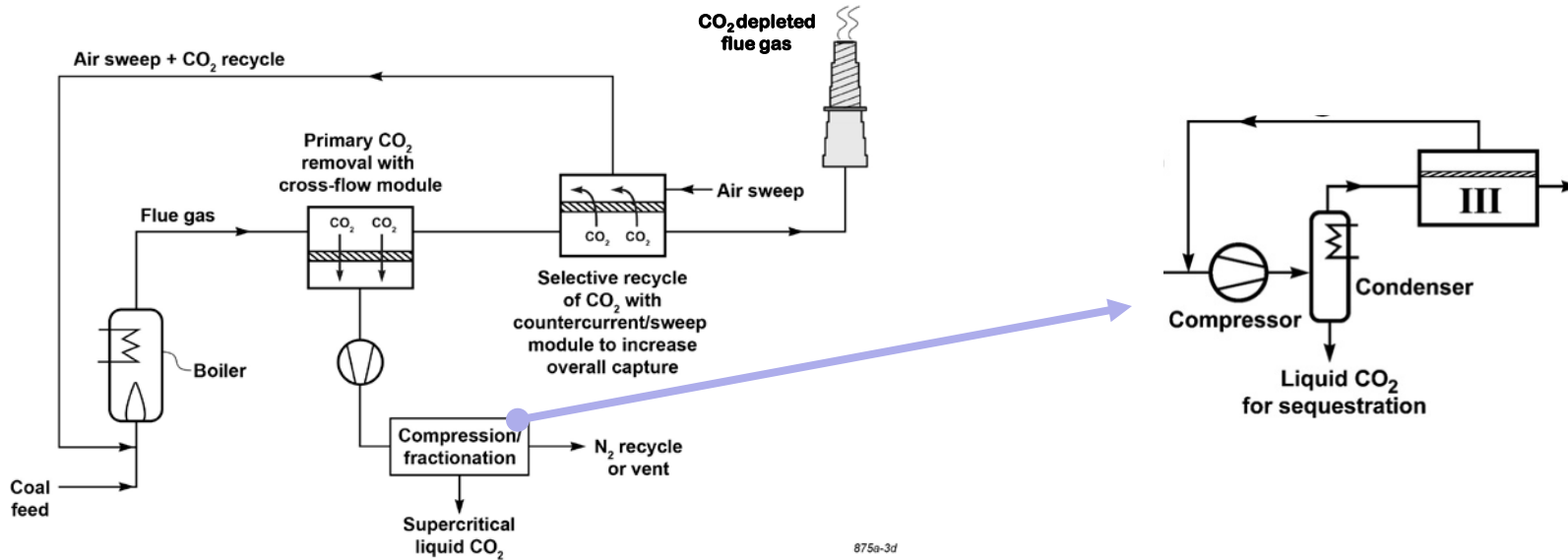
Viewpoint is from top of boiler looking down at flame



# Boiler Study Preliminary Findings

- Pilot-scale evaluation shows that stable flames can be obtained with sweep air (in fact B&W analysis indicates sweep flame is more stable due to additional combustion air swirl)
- Although flame is stable down to 16% O<sub>2</sub>, for existing boilers, 18% is preferred to minimize increased mass through boiler
- Data analysis to determine the effect of sweep air on boiler efficiency and the potential need for additional heat transfer surface area is ongoing
- Findings will be used to update BP1 techno-economic analysis

# CO<sub>2</sub> Liquefaction and Industrial Capture



- The compression/purification step of the flue gas CO<sub>2</sub> capture process uses a membrane-assisted refrigeration design
- This CO<sub>2</sub> liquefaction process was recently tested at NCCC (in a separate DOE-funded project) using the BP1 Polaris membrane
- In BP3, a similar membrane-assisted refrigeration process will be used to conduct a 1 TPD field test of CO<sub>2</sub> capture from a biowaste-to-methanol facility; the membrane performance will be compared with an existing Rectisol unit

# Summary

- Post-combustion capture membrane performance continues to improve
- Bench-scale slipstream tests at NCCC show membrane modules capable of generally stable 90% capture
- Many useful lessons learned from operating with real flue gas; NCCC assistance has been invaluable
- B&W CFD analysis and flame stability tests suggest CO<sub>2</sub> recycle with sweep membrane is feasible; detailed analysis ongoing
- Industrial CO<sub>2</sub> capture membranes have demonstrated liquid CO<sub>2</sub> production; industrial field tests planned
- Key objective of next 12 months is fabrication, installation, and operation of the 20 TPD demonstration unit

# Acknowledgements

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